

# Removal and recovery of NO by MnO<sub>2</sub>/Mg-Al layered double hydroxide

Tanya Kurutach<sup>1</sup>, Yuriko Takahashi<sup>1</sup>, Tomohito Kameda<sup>1</sup>\*, Shogo Kumagai<sup>1</sup>, Yuko Saito<sup>1</sup>,  
Keiichi Mizushima<sup>2</sup>, Ichiro Itou<sup>2</sup>, Tianye Han<sup>2</sup>, Toshiaki Yoshioka<sup>1</sup>

<sup>1</sup>Graduate School of Environmental Studies, Tohoku University, 6-6-07 Aoba, Aramaki, Aoba-ku, Sendai  
980-8579, Japan

<sup>2</sup>Kurita Water Industries Ltd., Nakano Central Park East, 4-10-1 Nakano, Nakano-ku, Tokyo 164-0001, Japan

\*corresponding author: tomohito.kameda@tohoku.ac.jp

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## INTRODUCTION

The incineration of waste generates exhaust gas containing poisonous nitrogen oxides (NO<sub>x</sub>). At present, Selective Catalytic Reduction (SCR) process is used for NO<sub>x</sub> removal. But treated product cannot be recycled and the high maintenance cost also become issue. Because of their capable of gas recovery and low price, CO<sub>3</sub>·Mg-Al layered double hydroxides (LDHs) has considerable attention in recent years. From anion exchange ability, they are used as adsorbent for nitrogen dioxide (NO<sub>2</sub>) removal, and adsorbed gases can be recovered in wet process<sup>1</sup>). However, they cannot remove nitric oxide (NO) contained more than 95 percent of NO<sub>x</sub> in exhaust gas<sup>1</sup>). Therefore, NO must be oxidized to NO<sub>2</sub> for removal. Transition metal oxides have high performances in NO oxidation. Mn based composite oxides are less expensive compared with others, and it has high activity in NO oxidation<sup>2</sup>). In this study, we investigated the performance of NO treatment by MnO<sub>2</sub>/Mg-Al LDH composite and MnO<sub>2</sub> + CO<sub>3</sub>·Mg-Al LDH mixture compared with CO<sub>3</sub>·Mg-Al LDH<sup>3-5</sup>). Additionally, NO removed by MnO<sub>2</sub>/Mg-Al LDH was examined to recover by thermal treatment.

## MATERIALS AND METHODS

### Preparation of MnO<sub>2</sub>/Mg-Al LDH

CO<sub>3</sub>·Mg-Al LDH (Mg/Al molar ratio = 2) was synthesized through co-precipitation and calcined at 500 °C for 2 h to yield Mg-Al oxide. Mg-Al oxide was added to KMnO<sub>4</sub> solution adjusted to Mn/Al molar ratios of 5 and stirred at 300 rpm and 30 °C. N<sub>2</sub> was bubbled into the solution throughout the procedure. After stirring for 6 h, solids were separated from the liquid and dried at 40 °C for 24 h, and MnO<sub>2</sub>/Mg-Al LDH was obtained. MnO<sub>2</sub>/Mg-Al LDH was analyzed by using X-ray diffraction (XRD), inductively coupled plasma-atomic emission spectrometry (ICP-AES), X-ray photoelectron spectroscopy (XPS).

### NO treatment

MnO<sub>2</sub>/Mg-Al LDH composite, MnO<sub>2</sub> + CO<sub>3</sub>·Mg-Al LDH mixture, or CO<sub>3</sub>·Mg-Al LDH were packed in reaction tube preheated to 170°C by electric tubular furnace. The mixed gas (NO: 150 ppm O<sub>2</sub>: 10%, N<sub>2</sub>: balance) was passed through the adsorbent for 90 min, with the flow rate adjusted by the mass flow controller (linear velocity 1.0 m/min). The residual concentrations were analyzed using a gas analyzer.

### NO recovery

NO removed by MnO<sub>2</sub>/Mg-Al LDH was recovered by thermal treatment. Firstly, desorbed temperature was analyzed via Evolved gas analysis-mass spectrometry (EGA-MS). MnO<sub>2</sub>/Mg-Al LDH had 1.33 mmol/g of NO,

and the materials were treated at 400-600°C using the above-mentioned apparatus.

## RESULTS AND DISCUSSION

### Preparation of MnO<sub>2</sub>/Mg-Al LDH

Figure 1 and Table 1 show the XRD patterns of the MnO<sub>2</sub>/Mg-Al LDH, and its chemical compositions. The XRD patterns indicate that LDH structure presents in the sample, while Mn species was not observed. But it contained 4.2 wt% of Mn, and basal spacing,  $d_{003}$ , was 7.6 Å. This suggests that MnO<sub>4</sub><sup>-</sup> was intercalated between the LDH layers. XPS analysis indicates that 76.7% of the Mn was Mn (IV). MnO<sub>4</sub><sup>-</sup>, intercalated between the LDH layers, was probably reduced to MnO<sub>2</sub> in the interlayer.

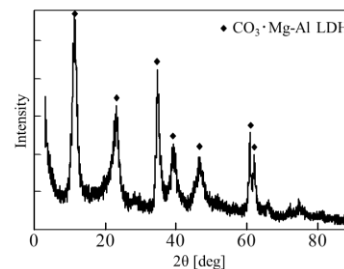


Figure 1 XRD patterns of the MnO<sub>2</sub>/Mg-Al LDH<sup>3)</sup>

### NO treatment

Table 2 shows the NO removal rates of the CO<sub>3</sub>·Mg-Al LDH, MnO<sub>2</sub>/Mg-Al LDH, and MnO<sub>2</sub> + CO<sub>3</sub>·Mg-Al LDH mixture. After 90 min, the NO removal rates of CO<sub>3</sub>·Mg-Al LDH, MnO<sub>2</sub>/Mg-Al LDH, and MnO<sub>2</sub> + CO<sub>3</sub>·Mg-Al LDH mixture are 0%, 1.4%, and 83.9% respectively. The NO removal rates of MnO<sub>2</sub>/Mg-Al LDH is notably higher than the others, indicating that a synergistic effect was generated when it becomes composite.

### NO recovery

EGA-MS result of MnO<sub>2</sub>/Mg-Al LDH after NO removal shows that NO peak was observed over 400 °C. NO recovery at 400-600 °C are shown in table 3. NO recovery performed at 600 °C presents 100% of recovery rate that significantly higher than 500 °C and 400 °C.

## CONCLUSION

NO treatment by MnO<sub>2</sub>/Mg-Al LDH composite has higher performance than CO<sub>3</sub>·Mg-Al LDH and MnO<sub>2</sub> + CO<sub>3</sub>·Mg-Al LDH mixture and denote 83.9% of removal rate. Moreover, trapped NO gas can be recovered 100 % at 600 °C.

## REFERENCES

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Table 1 Chemical compositions of MnO<sub>2</sub>/Mg-Al LDH<sup>4)</sup>

Mg/Al	Mn [wt%]	Mn/Al	CO <sub>3</sub> <sup>2-</sup> /Al	OH/Al
1.9	4.2	0.19	0.28	0.43

Table 2 NO removal rates of the CO<sub>3</sub>·Mg-Al LDH, MnO<sub>2</sub>/Mg-Al LDH, and MnO<sub>2</sub> + CO<sub>3</sub>·Mg-Al LDH mixture at 90 min<sup>5)</sup>

	CO <sub>3</sub> ·Mg-Al LDH	MnO <sub>2</sub> /Mg-Al LDH	MnO <sub>2</sub> + CO <sub>3</sub> ·Mg-Al LDH mixture
NO removal rate [%]	0	1.4	100

Table 3 NO recovery

	400°C	500°C	600°C
Recovery rate [%]	1.0	46.2	100